

MAHSA BABAEI<sup>1</sup>  
AFZAL KARIMI<sup>1</sup>  
MOHAMMAD AMIN HEJAZI<sup>2</sup>

<sup>1</sup>Department of Chemical  
Engineering, University of Tabriz,  
Tabriz, Iran

<sup>2</sup>Agriculture Biotechnology  
Research Institute of Iran,  
Northwest and West region, Tabriz,  
Iran

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## USE OF MESOPOROUS MnO<sub>2</sub> AS A SUPPORT FOR IMMOBILIZATION OF LIPASE FROM *Candida rugosa*

**Article Highlights**

- We used a new mesoporous carrier for immobilization of lipase from *Candida rugosa*
- The amount of enzyme loading on support was reached to 700 units per 1 g of support
- The thermal resistance of the enzyme was enhanced by immobilization
- The physical adsorption of enzyme to the support was strong

**Abstract**

In this study, immobilization of lipase from *Candida rugosa* on mesoporous manganese dioxide by adsorption was carried out and the effect of three immobilization variables including temperature, process time and enzyme/support ratio on immobilization efficiency were studied. The characteristics of synthesized MnO<sub>2</sub> and lipase-bound MnO<sub>2</sub> were investigated by scanning electron microscopy (SEM), transmission electron microscopy (TEM) and Fourier transform infrared spectroscopy (FT-IR) methods. The porous property of the support particles was also studied by X-ray diffraction (XRD) and Brunauer, Emmett and Teller (BET) measurements. The thermal stability of immobilized lipase was determined to be better than that of free enzyme. Also the operational stability of lipase-bound MnO<sub>2</sub> was studied and showed an almost strong attachment of enzyme to support. The Michaelis-Menten kinetic parameters ( $K_m$  and  $V_{max}$ ) were also determined for both free and immobilized lipases. It was observed that there is an increase of the  $K_m$  value (672.96 mg/ml) and a decrease of the  $V_{max}$  value (130.99 U/mg) for the immobilized enzyme comparing with the corresponding values of the free lipase.

**Keywords:** immobilization, *Candida rugosa* Lipase, physical adsorption, mesoporous manganese dioxide.

Lipases (triacylglycerol acylhydrolases, EC 3.1.1.3) are largely used as biocatalysts in biotechnology and modern chemistry [1]. These enzymes are also capable of catalyzing several reactions like esterification [2], transesterification (acidolysis, interesterification and alcoholysis), aminolysis, oximolysis, thio-transesterification and ammoniolysis in anhydrous organic solvents [3]. Considering the current high cost of lipases, it is necessary to use immobilization processes to make large-scale utilization of enzymatic reactions economically possible. Immobilization of enzymes can also change their secondary structure

leading to modification of their activity [4], better operation control, easier product recovery and flexibility of reactor design [5]. Aside from the application in industrial processes, the immobilization techniques are the basis for making a number of biotechnological products with applications in diagnostics, bioaffinity chromatography and biosensors. Therapeutic applications are also foreseen, such as the use of enzymes in extra-corporeal shunts [6].

Lipases can be immobilized on various supports by physical adsorption, covalent binding, ionic interactions or by entrapment [7]. Among these methods, adsorption of lipase onto insoluble support is the most commonly used approach because of its easy use and low cost. The forces between the support and the enzymes in this method include hydrogen bonding, van der Waals forces and hydrophobic interactions

Correspondence: A. Karimi, Department of Chemical Engineering, University of Tabriz, Tabriz, Iran.

E-mail: akarimi@tabrizu.ac.ir

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[8]. Lipase of *Candida rugosa* was adsorbed on different types of supports including synthetic or natural polymers [8-11], bentonite [12], kaolin [13], acrylic resins and textile membranes [14], glass beads [15] and magnetic beads [16].

Mesoporous MnO<sub>2</sub> is made up of nanoparticles with a large specific surface area that makes the high load of enzyme possible. There are certain requirements for the supports used in immobilization process that should be fulfilled to increase the efficiency of the process, such as large internal surface and high superficial density, and easy recovery of support at the end of process [17], which are all satisfied by utilizing MnO<sub>2</sub> as an immobilization host [18]. These characteristics have led MnO<sub>2</sub> nanoparticles to be successfully used in the fabrication of electrochemical biosensors [18,19]. In our previous work, MnO<sub>2</sub> nanoparticles were also successfully used as a support for immobilization of glucose oxidase [20].

In this study, lipase from *C. rugosa* was immobilized on mesoporous MnO<sub>2</sub> particles by physical adsorption. The manganese dioxide particles were characterized by scanning electron microscopy (SEM) and transmission electron microscopy (TEM). The adsorption of lipase onto MnO<sub>2</sub> particles was confirmed by Fourier transform infrared spectroscopy (FT-IR). The porous property of the support particles was also studied by X-ray diffraction (XRD) and Brunauer, Emmett and Teller (BET) measurements. The effects of three main immobilization variables (time, temperature and enzyme/support ratio) on process efficiency were studied. The properties of the immobilized lipase such as thermal and operational stability were also investigated.

## EXPERIMENTAL

### Materials

Lipase from *Candida rugosa* type VII (700 U/mg), sodium dihydrogen phosphate, di-sodium hydrogen phosphate, MnCl<sub>2</sub>, KMnO<sub>4</sub> and CCl<sub>4</sub> in the analytical grade were all purchased from Sigma Chemical Co.

### Preparation of mesoporous MnO<sub>2</sub>

Mesoporous MnO<sub>2</sub> was prepared according to the method described in our previous work [20]. 80 ml CCl<sub>4</sub> and 30 ml of 1 M MnCl<sub>2</sub> solutions were added to a container and made a biphasic system. 40 ml of 0.5 M KMnO<sub>4</sub> was added by two drops per second to the CCl<sub>4</sub> layer and upon reaching the interface, a brown material appeared at the interface. After 48 h, the brown MnO<sub>2</sub> was collected and washed with distilled water and ethanol for several times. The material was

then dried at 150 °C for 12 h, and stored for future use [21].

### Immobilization method

0.5 g of MnO<sub>2</sub> was dispersed in 10 ml of enzyme solution in 0.1 M sodium phosphate buffer, pH 7, and put into the shaker for a definite time at constant temperature. The resulting lipase-bound MnO<sub>2</sub> particles were separated by centrifuging and the supernatant was taken for activity analysis. The lipase-bound particles were washed with distilled water for several times to ensure that all the unbound lipases were washed off. The enzyme loading on support was calculated by the following equation [22]:

$$U_{\text{imm.}} = \frac{U_i - U_f}{m} \quad (1)$$

where  $U_{\text{imm.}}$  is the enzyme loading on support (U/g),  $U_i$  is the activity of enzyme in the attachment solution at the beginning of process and  $U_f$  is the activity of supernatant at the end of process, and m is the mass of support (g).

### Characterization of biocatalyst

The morphology and size of samples was studied by scanning electron microscopy (SEM) Leo 1455 VP model with 10 kV voltage, and by transmission electron microscopy (TEM) using the Philips CM120 at 100 kV. The FT-IR spectra of mesoporous MnO<sub>2</sub>, free lipase and lipase-bound MnO<sub>2</sub> was recorded by a Tensor 27 Model (Bruker German) spectrophotometer using KBr pellets. The X-ray diffraction (XRD) pattern of the mesoporous MnO<sub>2</sub> was determined using a D5000 diffractometer (Siemens German) with Cu K<sub>α</sub> radiation source ( $\lambda = 1.54056 \text{ \AA}$ ). The surface area and pore volume of the prepared MnO<sub>2</sub> were obtained through the Brunauer-Emmett-Teller (BET) with a Micromeritics Gemini 2375 (USA) analyzer.

### Enzyme activity assay

The hydrolytic activity of free and immobilized lipase was tested by olive oil hydrolysis [23]. The activity assay was carried out with reaction mixture containing 4 ml of olive oil and 5 ml of phosphate buffer (0.1 M, pH 7) in a 25 mL flask. The reaction was accomplished by adding a predetermined amount of free enzyme solution (1 mL) or supernatant (1 mL) or immobilized enzyme (0.1 g) to the mentioned reaction medium and shaking the flask at a constant temperature of 37 °C in a shaking incubator for 30 min. The liberated fatty acids were measured by titrating the flask content with 50 mM NaOH using a phenolphthalein indicator. One unit of lipase activity was

defined as the amount of enzyme that liberates 1  $\mu\text{mol}$  fatty acid per minute under the assay conditions [24]. All the activity assay experiments were repeated 3 times and the average amounts were used in calculations.

## RESULTS AND DISCUSSION

### Characterization of synthesized mesoporous $MnO_2$ particles

The morphology of  $MnO_2$  samples was studied by scanning electron microscopy (SEM) and transmission electron microscopy (TEM) as shown in Figure 1. According to the figure, the average size of particles is about 1  $\mu\text{m}$  and the porous property of  $MnO_2$  is obvious. Also from TEM image, the size of  $MnO_2$  particles is 38 nm length and 10 nm width.

Figure 2 shows the FT-IR spectra of lipase, the lipase-bound  $MnO_2$  and the uncoated  $MnO_2$ . As it can be seen in spectra of  $MnO_2$  particles, adsorption bands at  $521\text{ cm}^{-1}$  and  $602\text{ cm}^{-1}$  are related to Mn-O, and a band at  $3360\text{ cm}^{-1}$  indicates tension vibration of -OH with Mn atoms [20,25]. For the pure lipase, Amide I band corresponding to -CO carbonyl stretching mode of the peptide, is present in the region of  $1700\text{--}1600\text{ cm}^{-1}$  [26]. This band consists of a group of overlapped signals, which contain information on secondary protein structure of the enzyme. Bands centered at around  $1547\text{ cm}^{-1}$  are assignable to the amide II band, which is an out-of-phase combination mode of the NH in plane bend and the CN stretching vibration with smaller contributions from the CO in plane bend and the CC and NC stretching vibrations [27]. Finally, a set of bands can be distinguished in

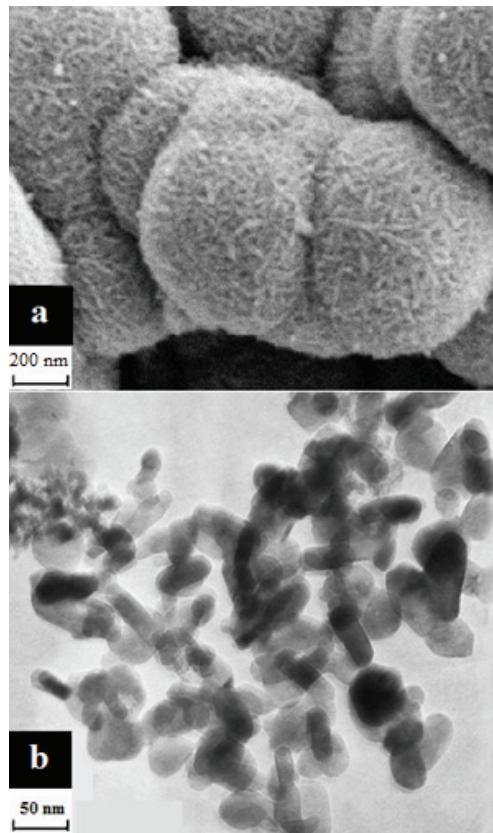


Figure 1. SEM (a) and TEM (b) images of the mesoporous  $MnO_2$  samples.

the region of  $1400\text{--}1200\text{ cm}^{-1}$  due to amide III mode. This mode is assigned to the in-phase combination of the NH deformation vibration with CN, with a minor contribution of CO and CC stretching [27]. The presence of amide I and amide III band of lipase enzyme in  $MnO_2$  particles can be clearly discerned by com-

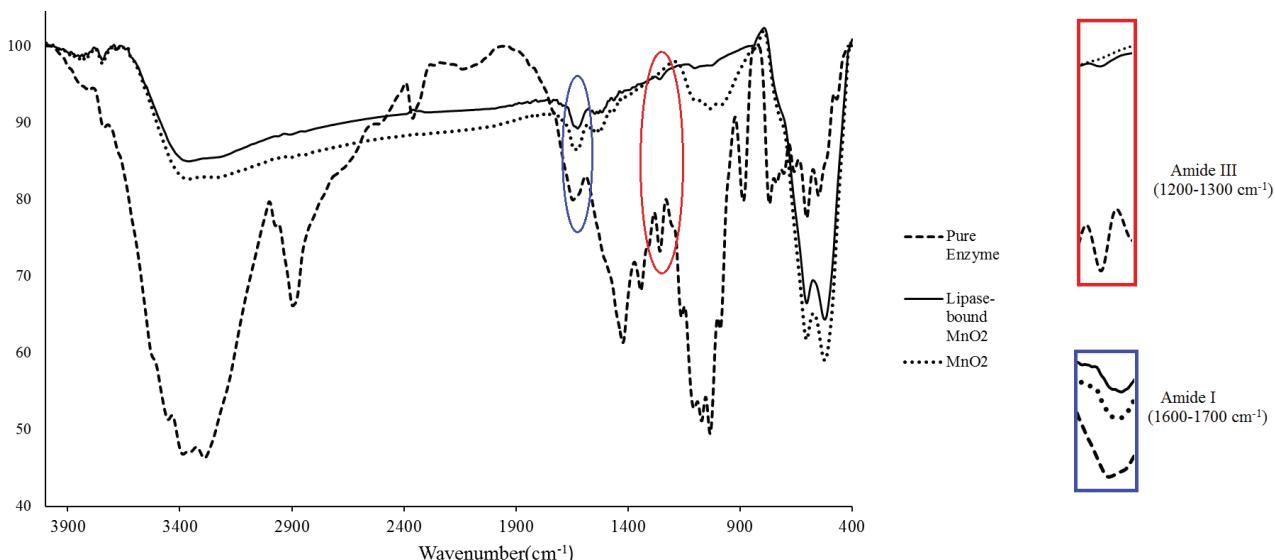


Figure 2. FT-IR Spectrum of pure lipase (blue), lipase-bound  $MnO_2$  (black) and  $MnO_2$  (red).

paring the spectra of lipase-bound MnO<sub>2</sub> with the one of uncoated MnO<sub>2</sub> in the region of about 1650 cm<sup>-1</sup> and 1269 cm<sup>-1</sup>, respectively (Figure 2). As it can be seen the band shape in lipase-bound MnO<sub>2</sub> is different from that of pure lipase, which indicates that some changes have occurred in the conformation of the enzyme after adsorption to the support. These conformational changes could be attributed to the loss of  $\alpha$ -helix structure and probable rising of  $\beta$ -sheet and/or self-aggregates [28].

The N<sub>2</sub> adsorption-desorption measurement using liquid N<sub>2</sub> (temperature of -196 °C) was performed to determine the mesoporosity and textural property of the MnO<sub>2</sub> sample (Figure 3a). Comparing the obtained isotherm to IUPAC classification proves that synthesized MnO<sub>2</sub> is of type IV with strong affinities [29-31].  $S_{\text{BET}}$ , the surface area of the sample calculated from the nitrogen isotherm using the BET method, was 176.93 m<sup>2</sup>/g and its total pore volume was 0.47 ml/g at  $P/P_0 = 0.99$ .

The X-ray diffraction pattern of the MnO<sub>2</sub> which was recorded at  $2\theta = 10$ -70° is illustrated in Figure 3b. Five distinct peaks are seen at  $2\theta$  values of: 25.1, 32.0, 37.1, 42.5, and 57.1°. A peak at  $2\theta = 32^\circ$  related to  $\gamma$ -MnO<sub>2</sub> (JCPDS 14-0644), peaks at  $2\theta = 25.1$  and 37.1° represent  $\alpha$ -MnO<sub>2</sub> (JCPDS 44-0141), and peaks at  $2\theta = 42.5$  and 57.1° illustrate  $\beta$ -MnO<sub>2</sub> (JCPDS 24-0735) [32,33]. So the synthesized MnO<sub>2</sub> crystalline state is a combination of  $\alpha$ ,  $\beta$  and  $\gamma$ -MnO<sub>2</sub>.

The spacing distance between crystals was calculated from the Scherer equation:

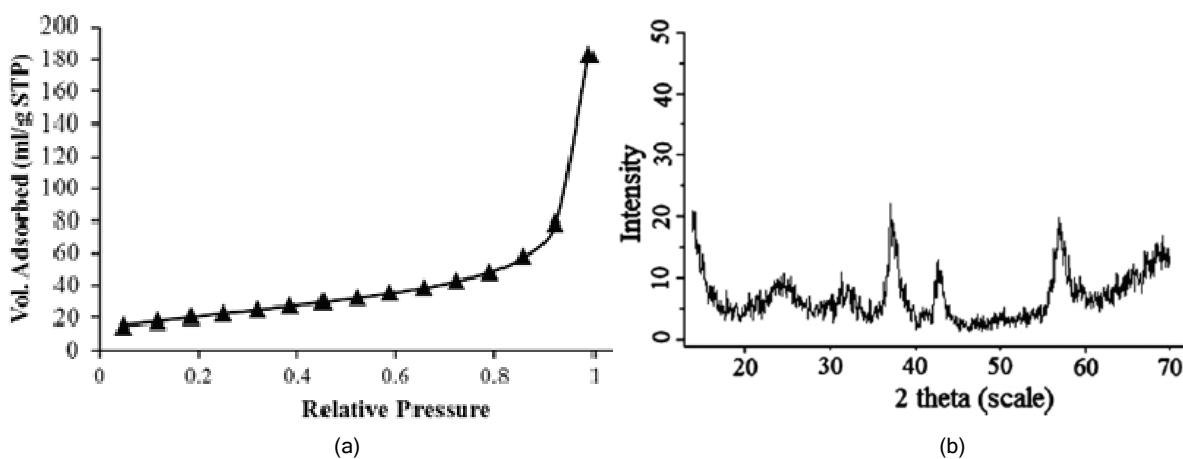


Figure 3. Nitrogen adsorption isotherm of the synthesized MnO<sub>2</sub> (a), and XRD pattern of the mesoporous MnO<sub>2</sub> (b).

Table 1. Crystalline XRD properties of the synthesized MnO<sub>2</sub>

Deffraction angle (2θ / °)	Intensity	Average size of MnO <sub>2</sub> crystal $d_c$ , nm	Distance between adjacent pore centers, $a$ / nm
37.10	25	10.52	12.15
43.12	15	11.83	13.66
56.68	24	7.59	8.77

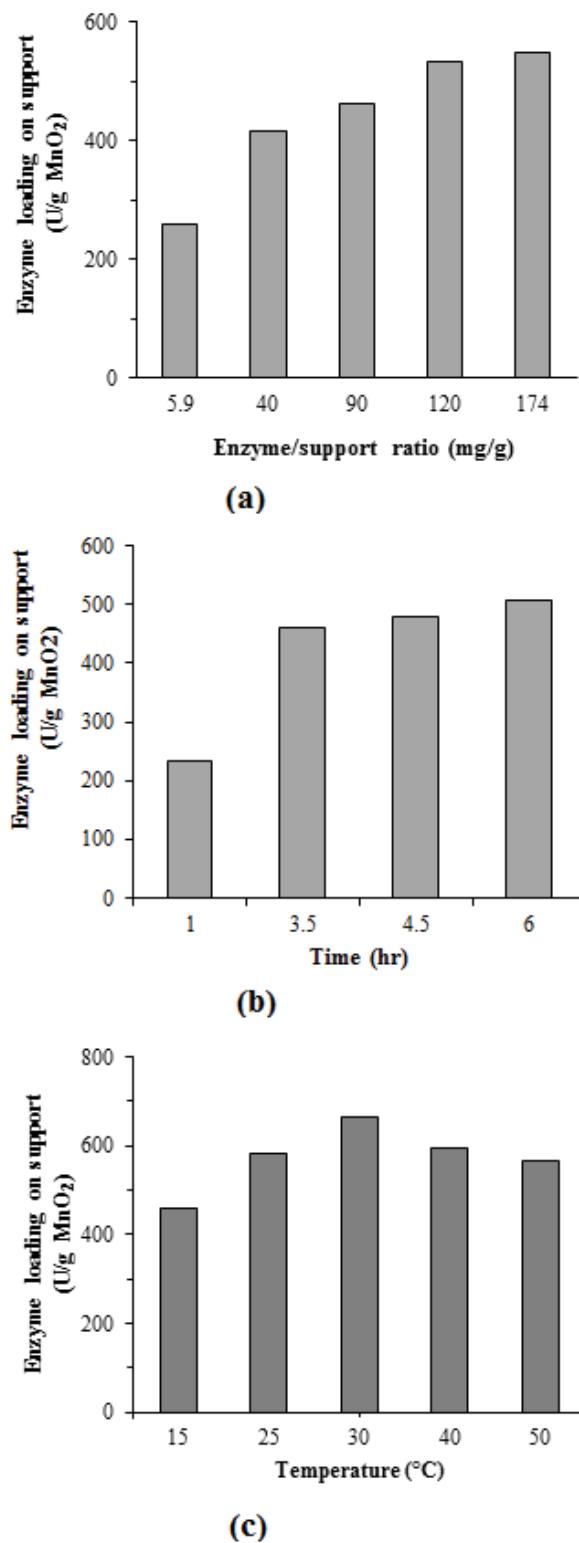


Figure 4. The effect of enzyme/support ratio (a), immobilization time (b) and temperature (c) on enzyme loading on MnO<sub>2</sub>.

1 g of support reaches to 530 U. Further increasing of this ratio to 174 mg/g accounts to loaded enzyme addition of only 20 U. This means that by introducing 45% more enzymes to the attachment solution, the

amount of enzyme loading on support was only increased by 3.7%. It can be predicted that by increasing enzyme/support ratio, there would be no significant raise in immobilization amount due to the saturation of active sites of support by enzyme.

#### Immobilization process time

The effect of immobilization process time on the efficiency of immobilization of lipase from *C. rugosa* was studied by carrying the process with enzyme/support ratio of 90 mg/g at 15 °C for different immobilization time of 1-6 h. The results are shown in Figure 4b. It can be seen that by increasing immobilization process time from 1 to 3.5 h, the amount of enzyme loaded on support is doubled. However, by continuing the immobilization process for another 2.5 h, the amount of enzyme loading on support was increased by only 8.7%. Considering the energy consumed during this additional time of 2.5 h and insignificant amount of enzyme loading gain of 8.7%, it is not reasonable to continue the process over 3.5 h. Also by increasing immobilization time, the protein conformation of lipase might denature and result in activity decrease and limitation of immobilization process [34].

#### Immobilization process temperature

The amount of heat energy that is introduced to the immobilization system is an important parameter. Increasing the temperature improves the accessibility and mobility of enzyme, but over a certain temperature, it would lead to the possible inactivation of enzyme by thermal denaturation. Therefore the immobilization process was carried out with enzyme/support ratio of 90 mg/g for 3.5 h at different temperatures ranging 15-50 °C, to find the optimum temperature. The results are shown in Figure 4c. It can be seen that the highest enzyme loading on support was achieved by running the immobilization process at 30 °C.

#### Effect of temperature on activity of free and immobilized enzymes

The effect of temperature on activity of both free and immobilized lipase was studied in the range of 25-60 °C as shown in Figure 5. It is obvious that the activity of free lipase is very dependent on temperature and the maximum amount of activity is observed at approximately 35-40 °C, while it shifts to a wider range of 35-45 °C for the immobilized lipase. The increase in optimum temperature range might be a result of reduced conformational flexibility that demands higher activation energy for the molecule to reorganization the proper conformation for binding to substrate [35]. One of the main advantages of enzyme immobilization is the mentioned increase in its

stability due to restricted conformational mobility of the protein molecule. Comparing the rate of activity loss for immobilized lipase from *C. rugosa* to the corresponding profiles of other carriers like magnetic microspheres [36] and sol-gel support [1] shows that lipase-bound  $\text{MnO}_2$  retains 10 and 30% more activity at 60 °C, respectively.

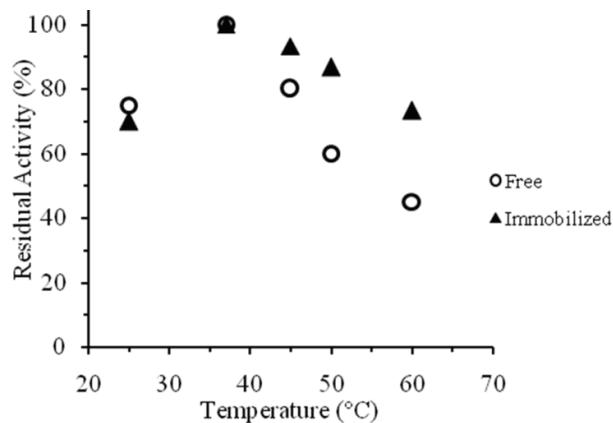


Figure 5. The effect of temperature on the relative activity of the free and immobilized enzymes.

#### Reusability and operational stability of free and immobilized enzymes

Reusing the immobilized enzyme requires strong attachment of lipase to the support to assure activity retaining after several operations. To investigate whether the lipase-bound  $\text{MnO}_2$  holds its catalytic activity during several operation, the immobilized particles were incubated at 37 °C in a flask containing 4 ml of olive oil and 5 ml of phosphate buffer (0.1 M, pH 7) for 30 min. The amount of lipase enzyme bound to the support is directly proportional to the yield of hydrolysis reaction in the flask. The biocatalyst particles were separated by filtration, and the flask content was analyzed by titrating. The separated lipase-bound

$\text{MnO}_2$  particles were washed with phosphate buffer solution (0.1 M, pH 7) and used again to catalyze the aforementioned hydrolysis reaction. This procedure was repeated for 6 times and the results were presented in Table 2. After 6 times of reusing, reduction of activity was 30%. This would be caused by leakage of protein from support upon washing.

Table 2. Strength of lipase attachment to the  $\text{MnO}_2$

Number of reusing	0	1	2	3	4	5	6
Residual activity, %	100	92.5	87.5	82.5	75	72.5	70

#### Thermal stability of free and immobilized enzymes

The thermal stability of immobilized enzyme is one of the important criteria for its application. The activity of immobilized enzyme must be more resistant than that of the free form against heat and denaturing agents. This was studied by incubating both free and immobilized enzyme in phosphate buffer (0.1 M, pH 7) at 50 °C. The activity of both free and immobilized enzyme decreased during the time, whereas the activity of lipase-bound  $\text{MnO}_2$  decreased more slowly than the free one (Figure 6). It can be seen that the free enzyme lost its activity during 2.5 h of incubation period, but the activity loss of immobilized one is only 3% during the same time. Immobilized lipase was inactivated at a much slower rate than that of the free form, that the immobilized enzyme retains 71% of its initial activity after 14 h. This could be explained by the protein-surface interaction in immobilized enzyme that protects it from unfolding and prevents the conformation transition of the enzyme at high temperatures [31,37].

#### Kinetic parameters

The kinetics of simple enzyme catalyzed reactions can be determined by Michaelis-Menten equation. To determine the Michaelis-Menten kinetic para-

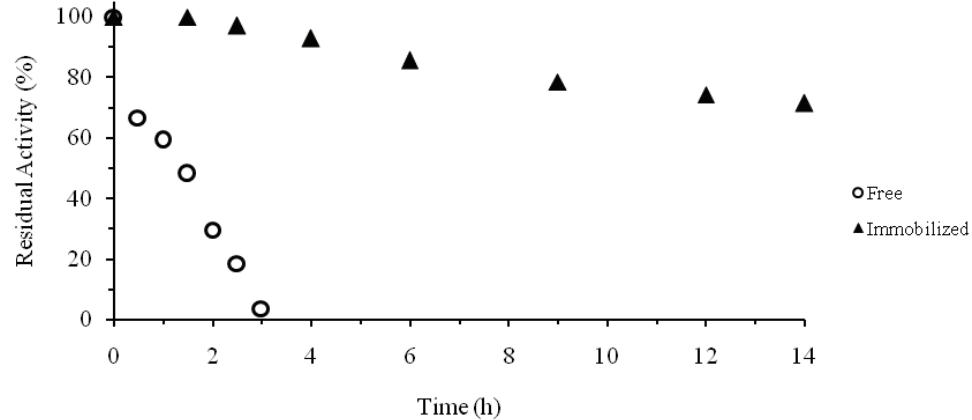


Figure 6. Stability of the free and immobilized lipase at 50 °C.

meters ( $K_m$  and  $V_{max}$ ) for both free and immobilized lipase, different concentrations of olive oil over the range of 0.2–0.85 g/ml were used and the activities were measured. The parameters were calculated by the Lineweaver-Burk method as follows:

$$\frac{1}{v} = \left\{ \left[ \frac{K_m}{V_{max}} \right] \left[ \frac{1}{S} \right] \right\} + \frac{1}{V_{max}} \quad (3)$$

A plot of  $v$  against  $1/S$  will give a straight line with the slope of  $K_m/V_{max}$  and an intercept on the ordinate at  $1/V_{max}$  as shown in Figure 7. The Michaelis-Menten constants  $K_m$  and  $V_{max}$  were calculated as 131.93 mg/ml and 280.96 U/mg protein for free lipase, and 804.89 mg/ml and 149.97 U/mg support for immobilized lipase, respectively. The attachment of enzyme molecule to the support by means of non-covalent forces (hydrogen bonds, ionic, and van der Waals interactions) leads to a reduction of molecular mobility. Also, the immobilization of enzyme limits the accessibility of substrate to reach the active sites of enzyme. These all result in an increase of  $K_m$  value during the immobilization process. However, the aforementioned structural changes of lipase enzyme due to immobilization procedure improve the enzyme resistance to changes of temperature, pH and enhances its lifetime significantly [38]. As a result, the lower reaction rate of immobilized enzyme is still considered more economical.

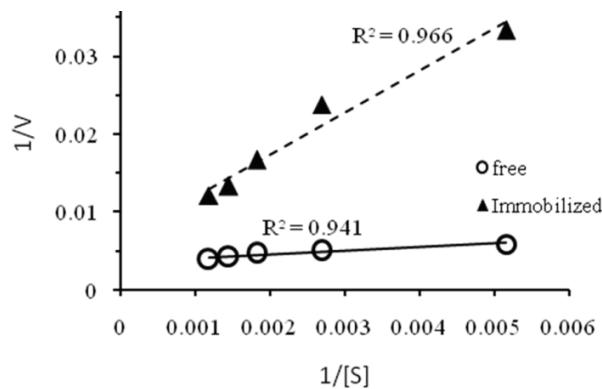


Figure 7. Lineweaver-Burke lines for free and immobilized lipase.

## CONCLUSION

In the present work, lipase from *Candida rugosa* was immobilized on mesoporous MnO<sub>2</sub> by physical adsorption and the effect of different immobilization variables were studied. The best result of the immobilization process was achieved at enzyme/support ratio of 120 mg/g, immobilization temperature of 30 °C, and incubation time of 3.5 h. In addition, the

immobilized enzyme exhibited better resistance to temperature inactivation and thermal stability than the free form. The reusability of the immobilized enzyme was studied, showing that it retained 70% of its initial activity after 6 times of reutilizing. By applying the Michaelis-Menten equation for the lipase catalyzed reaction, the  $K_m$  value for immobilized lipase was determined to be higher than that of the free one. This shows that the rate of immobilized-lipase catalyzed reaction is lower than free lipase. However, the thermal and operational stability of immobilized lipase makes the immobilized lipase more suitable for industrial and large-scale operations. Considering the simplicity and low cost of the immobilization process, it can be concluded that mesoporous MnO<sub>2</sub> is an efficient carrier for lipase immobilization.

## REFERENCES

- [1] A. Uyanik, N. Sen, M. Yilmaz, Bioresour. Technol. **102** (2011) 4313-4318
- [2] A.R.M. Yahya, W.A. Anderson, M.M. Young, Enzyme Microb. Technol. **23** (1998) 438-450
- [3] P. Villeneuve, J.M. Muderhwa, J. Graille, M.J. Haas, J. Mol. Catal., B **9** (1999) 113-148
- [4] S.E. Collins, V. Lassalle, M.L. Ferreira, J. Mol. Catal., B **72** (2011) 220-228
- [5] P.V. Iyer, L. Ananthanarayan, Process Biochem. **43** (2008) 1019-1032
- [6] B.M. Brena, F.B. Viera, J. Mol. Catal. B: Enzym. **65** (2006) 102-109
- [7] E. Yilmaz, K. Can, M. Sezgin, M. Yilmaz, Bioresour. Technol. **102** (2011) 299-506
- [8] H. Tutar, E. Yilmaz, E. Pehlivan, M. Yilmaz, Int. J. Biol. Macromol. **45** (2009) 315-320
- [9] G. Kamel, F. Bordi, L. Chronopoulou, S. Lupi, C. Palocci, S. Sennato, P.V. Verdes, Surf. Sci. **605** (2011) 2017-2024
- [10] Z.G. Wang, J.Q. Wang, Z.K. Xu, J. Mol. Catal., B **42** (2006) 45-51
- [11] M.A. Geluk, W. Norde, H.K. Kalsbeek, K.V. Riet, Enzyme Microb. Technol. **14** (1992) 748-754
- [12] Y. Yesiloglu, Process Biochem. **40** (2005) 2155-2159
- [13] M.B. Rahman, S.M. Tajudin, M.Z. Hussein, R.N. Rahman, A.B. Salleh, M. Basri, Appl. Clay Sci. **29** (2005) 111-116
- [14] T. Tan, J. Lu, K. Nie, L. Deng, F. Wang, Biotechnol. Adv. **28** (2010) 628-634
- [15] E. Yilmaz, K. Can, M. Sezgin, M. Yilmaz, Bioresour. Technol. **102** (2011) 499-506
- [16] M.P. Marszall, T. Siódmiak, Catal. Commun. **24** (2012) 80-84
- [17] C. Mateo, J.M. Palomo, G.F. Lorente, J.M. Guisan, F.R. Lafuente, Enzyme Microb. Technol. **40** (2007) 1451-1463

- [18] J. Yu, T. Zhao, B. Zeng, *Electrochim. Commun.* **10** (2008) 1318-1321
- [19] E. Turkusic, J. Kalcher, E. Kahrovic, N.W. Beyene, H. Moderegger, E. Sofic, S. Begic, K. Kalcher, *Talanta* **65** (2005) 559-564
- [20] A. Karimi, F. Mahdizadeh, D. Salari, A. Niaezi, *Desalination* **275** (2011) 148-153
- [21] C. Yuan, B. Gao, L. Su, X. Zhang, *J. Colloid Interface Sci.* **322** (2008) 545-550
- [22] A. Salis, M. Pinna, M. Monduzzi, V. Solinas, *J. Mol. Catal. B: Enzym.* **54** (2008) 19-26
- [23] W. Xie, N. Ma, *Biomass Bioenergy* **34** (2010) 890-896
- [24] S.W. Chang, J.F. Shaw, K.H. Yang, S.F. Chang, C.J. Shieh, *Bioresour. Technol.* **99** (2008) 2800-2805
- [25] M. Voinov, *Electrochim. Acta* **27** (1982) 833-835
- [26] Barth, *Biochim. Biophys. Acta* 1767 (2007) 1073-1101
- [27] J. Kong, S. Yu, *Acta Biochim. Biophys. Sin.* **39** (2007) 549-559
- [28] P.I. Haris, F. Sevencan, *J. Mol. Catal. B: Enzym.* **7** (1999) 207-221
- [29] G. Fagerlund, *Mater. Struct.* **6** (1973) 239-245
- [30] K.S. Ramsay, W. Sing, K.K. Unger, *Pure Appl. Chem.* **66** (1994) 1739-1758
- [31] R. Scherer, J.V. Oliveira, S. Pergher, D. Oliveira, *Mat. Res.* **14** (2011) 483-492
- [32] S. Devaraj, N. Munichandraiah, *J. Phys. Chem.* **112** (2008) 4406-4417
- [33] Y. Yang, L. Xiao, Y. Zhao, F. Wang, *Int. J. Electrochem. Sci.* **3** (2008) 67-74
- [34] D.S. Jiang, S.Y. Long, J. Huang, H.Y. Xiao, J.Y. Zhou, *Biochem. Eng. J.* **25** (2005) 15-23
- [35] M.Y. Arica, G. Bayramoglu, N. Bicak, *Process Biochem.* **39** (2004) 2007-2017
- [36] Y. Yong, Y.X. Bai, Y.F. Li, L. Lin, Y.J. Cui, C.G. Xia, *Process Biochem.* **43** (2008) 1179-1185
- [37] F. Xi, J. Wu, Z. Jia, X. Lin, *Process Biochem.* **40** (2005) 2833-2840
- [38] M. Miroliae, *Sci. Iran.* **14** (2007) 112-117.

MAHSA BAAEI<sup>1</sup>  
AFZAL KARIMI<sup>1</sup>  
MOHAMMAD AMIN HEJAZI<sup>2</sup>

<sup>1</sup>Department of Chemical Engineering,  
University of Tabriz, Tabriz, Iran  
<sup>2</sup>Agriculture Biotechnology Research  
Institute of Iran, Northwest and West  
region, Tabriz, Iran

NAUČNI RAD

## PRIMENA MEZOPOROZNOG MnO<sub>2</sub> KAO NOSAČA ZA IMOBILIZACIJU LIPAZE *Candida rugosa*

*U ovom radu izvršena je imobilizacija lipaze *Candida rugosa* na mezoporoznom magnan-dioksidu adsorpcionom metodom. Ispitan je uticaj temperature, vremena trajanja procesa i odnosa enzim/nosač na efikasnost imobilizacije. Karakteristike sintetizovanog MnO<sub>2</sub> i MnO<sub>2</sub> vezanog za enzim su ispitane metodama skenirajuće elektronske mikroskopije (SEM), transmisione elektronske mikroskopije (TEM) i infracrvene spektroskopije sa Furijevom transformacijom (FT-IR). Poroznost nosećih čestica je ispitana difrakcijom X-zraka (XRD) i BET metodom. Utvrđeno je da je termalna stabilnost imobilisane lipaze bolja u odnosu na termalnu stabilnost slobodnog enzima. Na osnovu ispitivanja operacionih stabilnosti dokazana je jaka veza enzima i nosača. Određeni su kinetički parametri Michaelis-Menten jednačine ( $K_m$  i  $V_{max}$ ) za slobodnu i imobilisanu lipazu. Utvrđeno je da postoji povećanje vrednosti  $K_m$  (672,96 mg/ml) i opadanje vrednosti  $V_{max}$  (130,99 U/mg) kod imobilisanog enzima u odnosu na vrednosti kod slobodne lipaze.*

*Ključne reči:* Imobilizacija, lipaza *Candida rugosa*, fizička adsorpcija, mesoporozni mangani-dioksid.